

Seventh Annual Conference on Carbon Capture & Sequestration

Relative Permeability Properties of the CO₂/Brine System in Saline Aquifers: An Experimental Study

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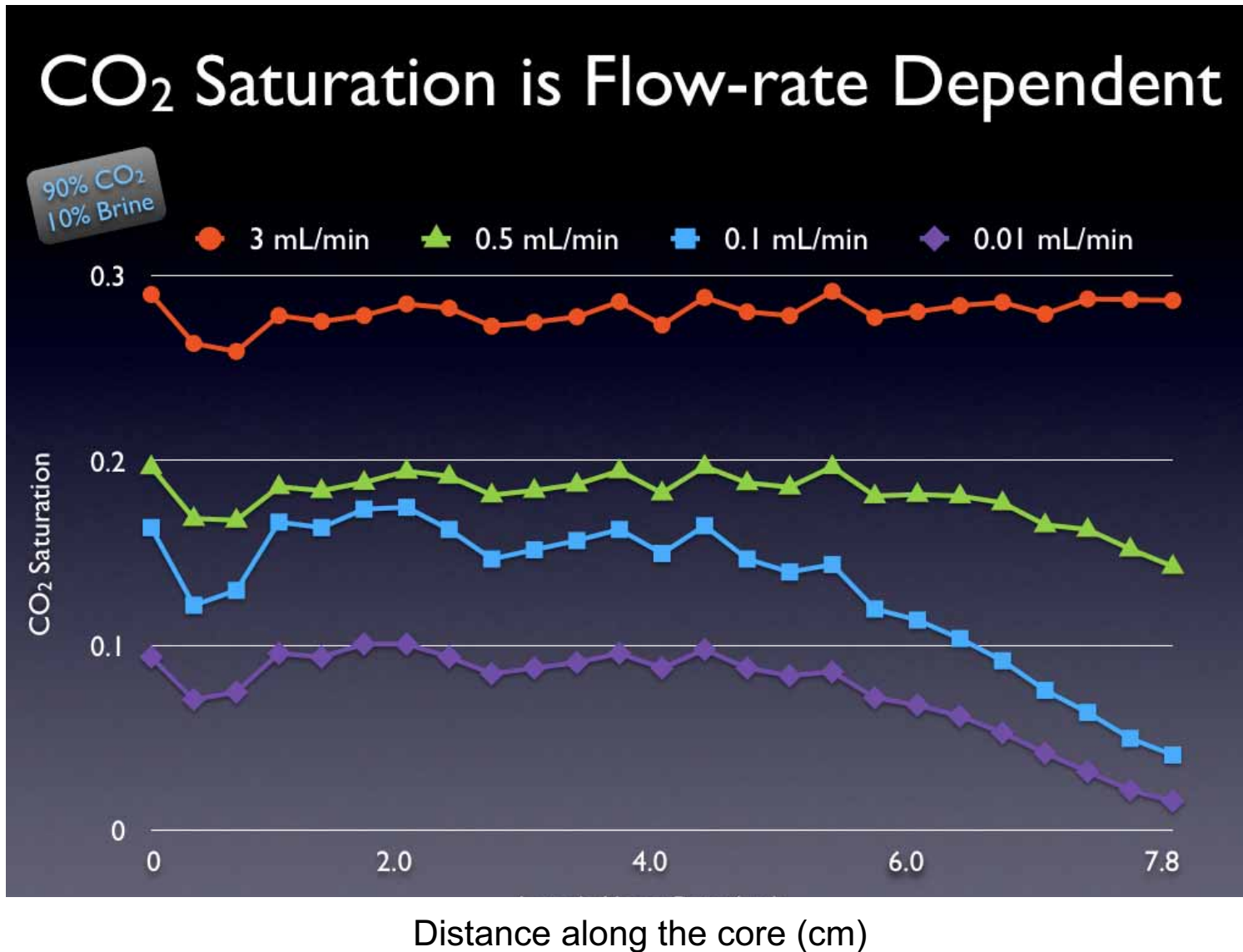
Stanford University

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- OVERVIEW -

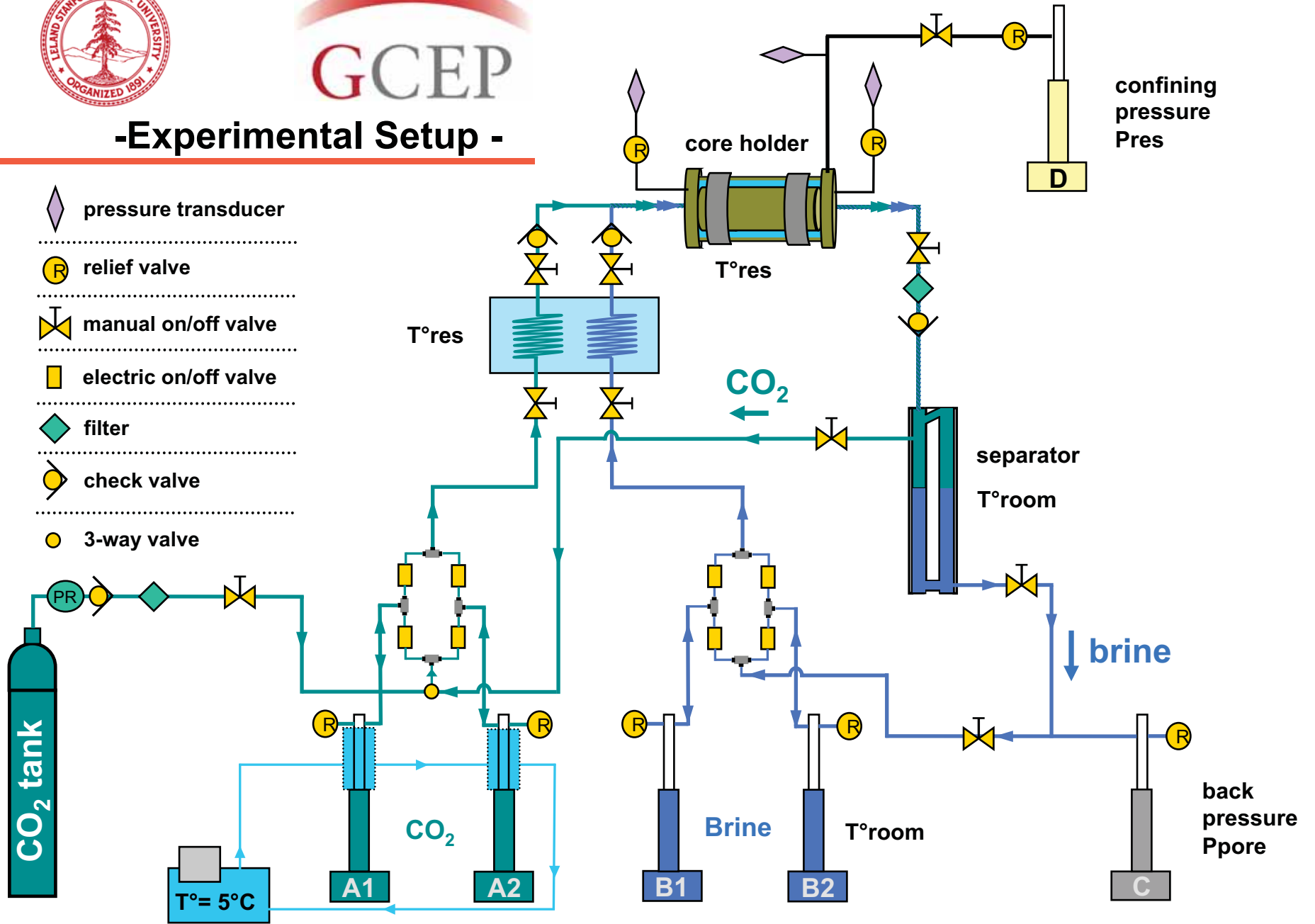
- Motivations
- Experimental Setup
- Core characterization
- 2-phase flow : experimental conditions/procedure
- Results
- Conclusions

- MOTIVATIONS -





-Experimental Setup -

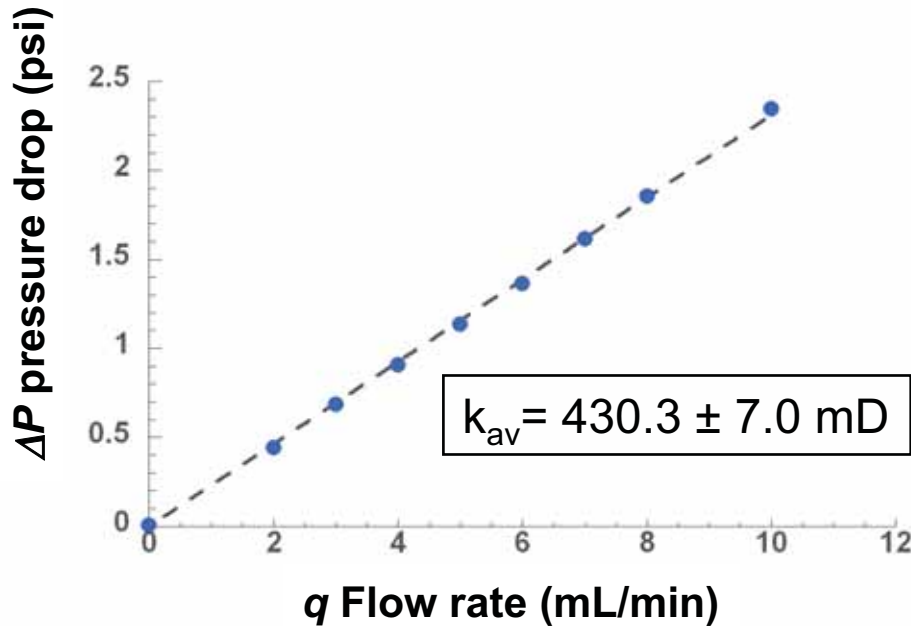
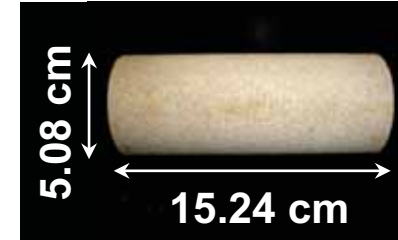




– Core characterization – Absolute Permeability



- Sample = Berea Sandstone
- Absolute permeability:
 - Injection of brine (10 000 ppm NaCl \approx 10 g/L)
 $T^\circ = 50^\circ\text{C}$, $P_{\text{pore}} = 12.4 \text{ MPa}$
 - Measure ΔP as a function of the Flow Rate q

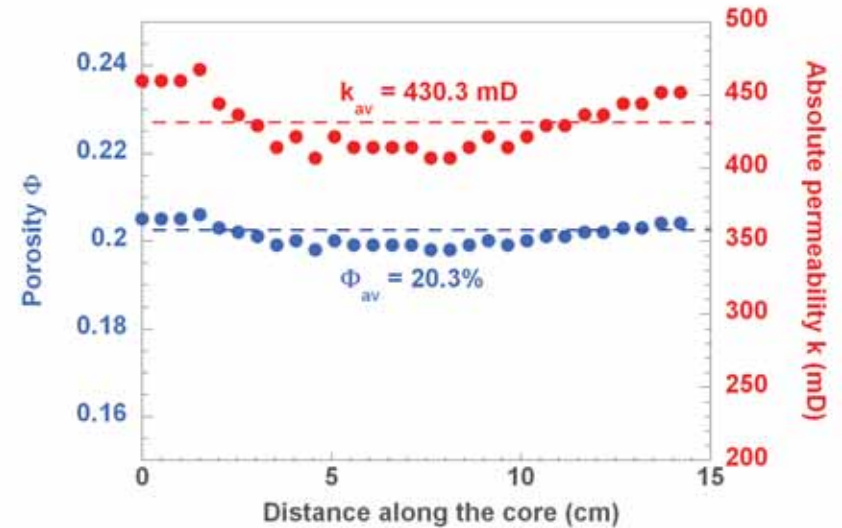
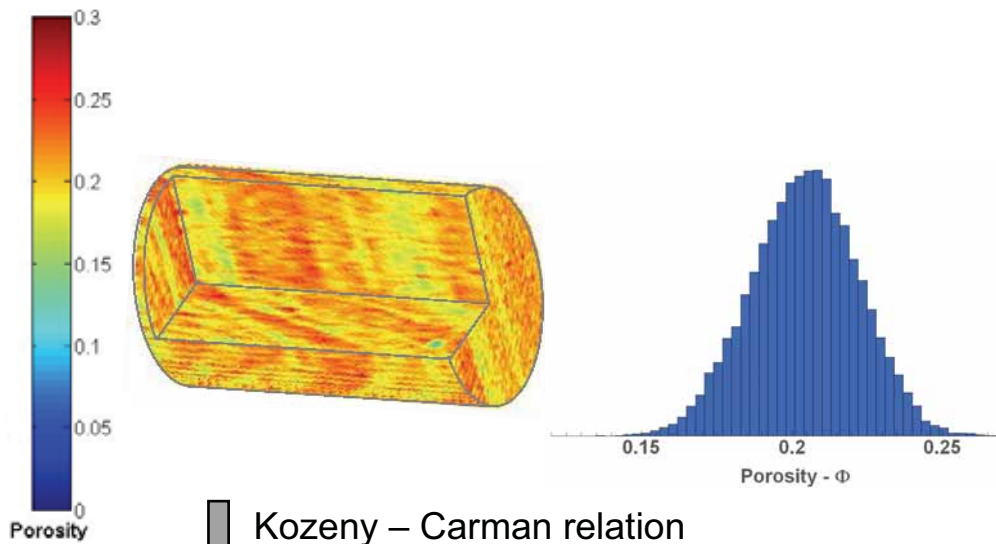


$$\Delta P = \frac{1}{k} \underbrace{\frac{L\mu}{A}}_{\text{known coefficient}} q$$

$$A = 40.53 \text{ cm}^2$$
$$L = 15.24 \text{ cm}$$
$$\mu = 0.54 \text{ cp}$$

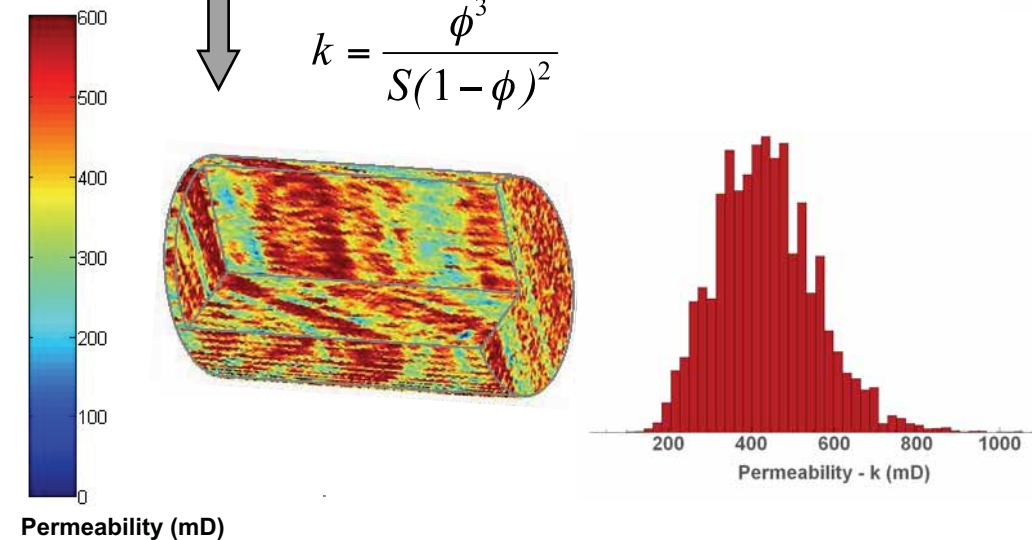


– Core characterization – Porosity, Permeability



Kozeny – Carman relation

$$k = \frac{\phi^3}{S(1-\phi)^2}$$



Porosity and permeability have important spatial variations due to the pore-scale structure of the rock sample.

The slice-averaged values are relatively constant along the core.



– 2-phase flow experiments – Experimental conditions



- Co-injection of supercritical CO₂ and brine at reservoir conditions:

T° = 50°C
P_{pore} = 12.4 MPa

→ corresponds to a depth of 1700 m
(for $\nabla T^\circ = 0.3^\circ\text{C}/100\text{m}$ and $\nabla P = 820\text{ kPa}/100\text{m}$)

- Physical properties of CO₂ and brine at reservoir conditions:

CO₂ saturated brine	CO₂
Liquid $\mu = 0.558\text{ cP}$ $d = 0.990\text{ g/cm}^3$	Supercritical $\mu = 0.046\text{ cP}$ $d = 0.28\text{ g/cm}^3$

Viscosity ratio $\nu = \mu_{\text{brine}} / \mu_{\text{CO}_2} = 12.1$

Density ratio $d_{\text{brine}} / d_{\text{CO}_2} = 3.5$

Bond number ~ 0.2

Capillary number $\sim [2 \cdot 10^{-6} - 10^{-5}]$



– 2-phase flow experiments – Experimental procedure



- At a given total Flow Rate $FR(CO_2) + FR(brine)$:
 - the core is initially saturated with brine
 - CO_2 and brine are injected at a *given fractional flow*

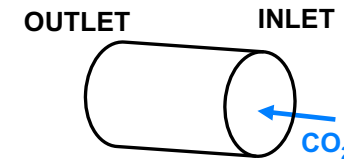
$$f_{brine} = \frac{FR(brine)}{FR(CO_2) + FR(brine)}$$

$$f_{CO_2} = \frac{FR(CO_2)}{FR(CO_2) + FR(brine)}$$

- wait until steady state is reached (**HOW LONG?**)
 - stabilization of pressure drop and saturation
- measure ΔP , saturation
- increase the proportion of CO_2 ($f_{CO_2} \uparrow$)

- Run the same procedure at different total flow rates: 2.6, 1.2 and 0.5 mL/min

Injection of 100% CO₂ @ 2mL/min



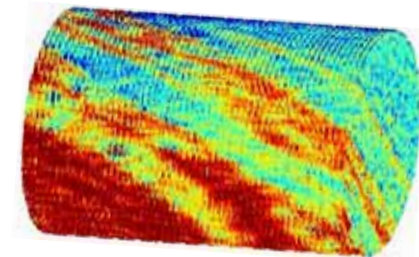
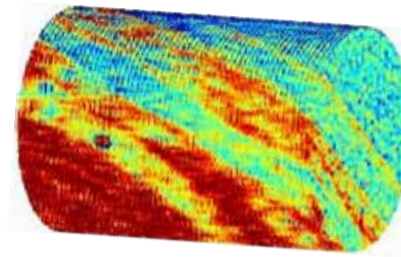
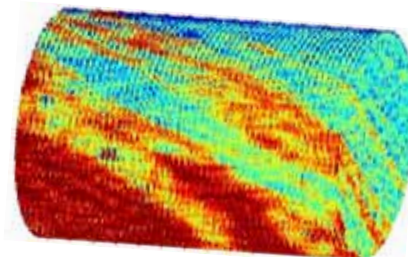
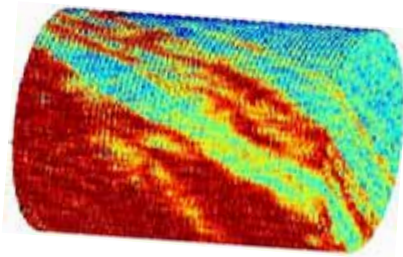
pore volumes

0.88

2.06

3.38

5.29



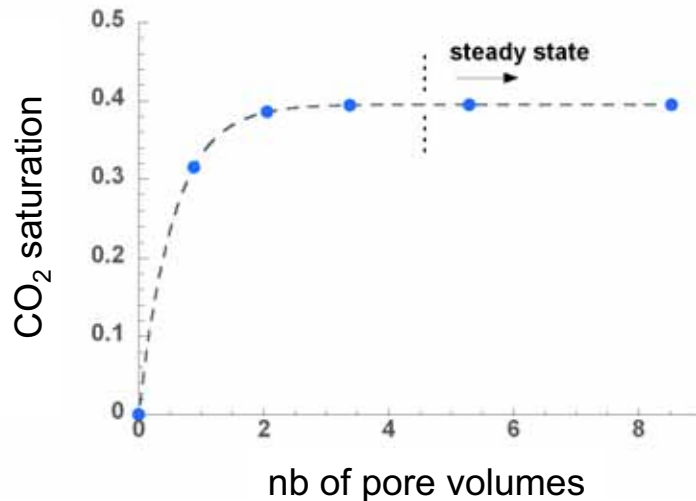
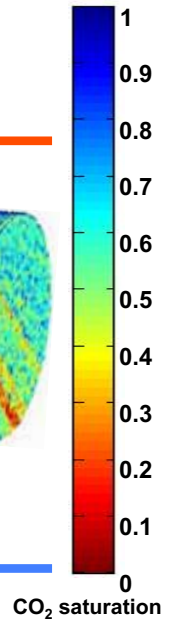
S_{CO_2}

0.315

0.387

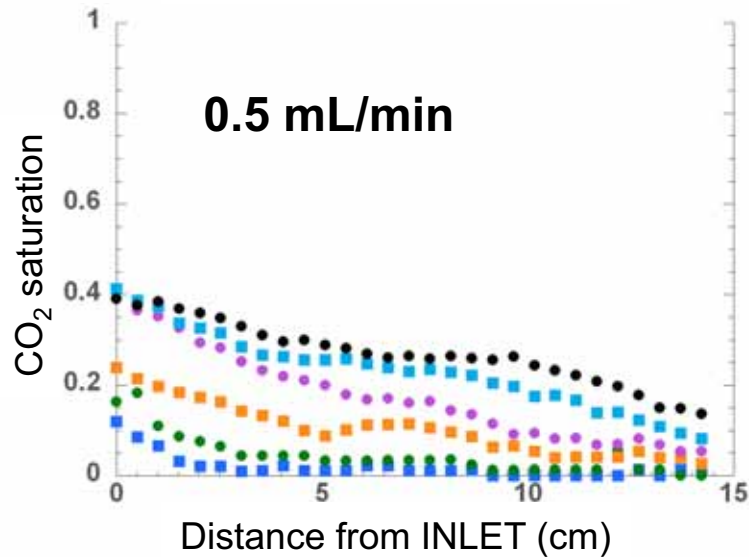
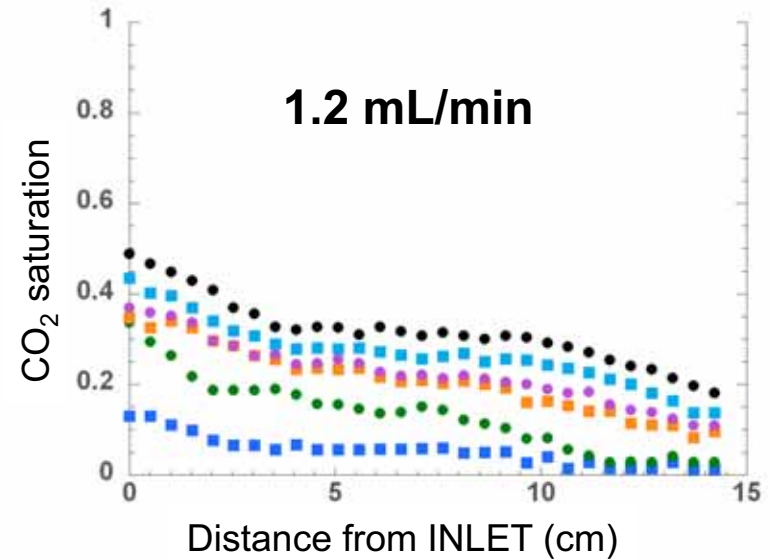
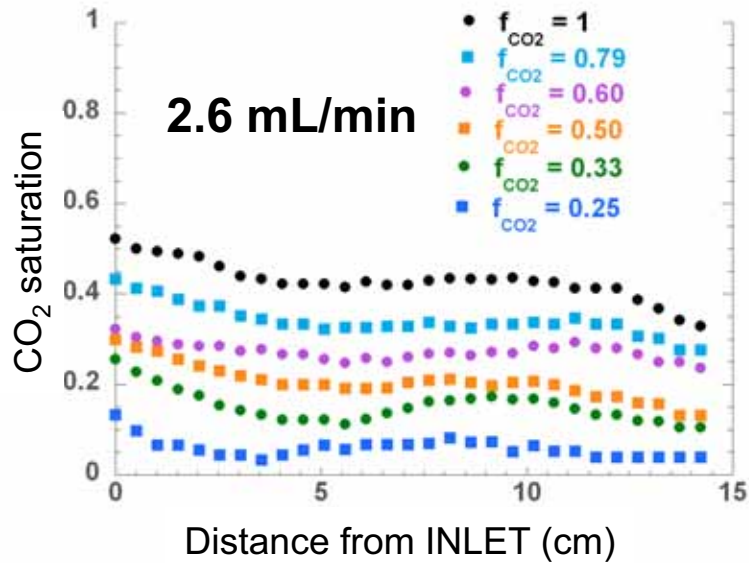
0.394

0.395



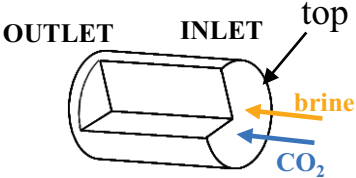
- The steady state is reached after ~ 5 pore volumes
- To be sure to always reach steady state DP and S_{CO_2} are measured after having injected 8-10 pore volumes of fluid.

- Results - CO₂ saturation at different fractional flow



- The higher the proportion of CO₂, the higher the CO₂ saturation.
- Lower values when the flow rate decreases.

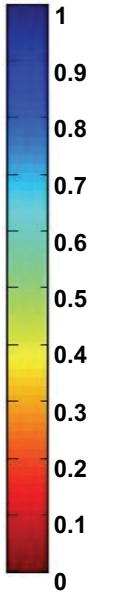
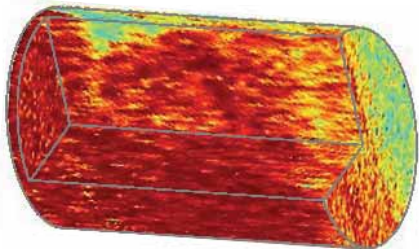
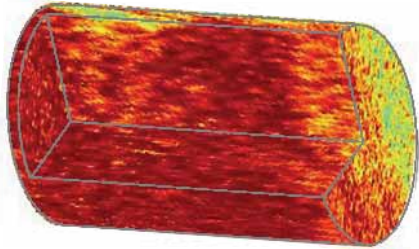
- Results -
 Total flow rate = 2.6 mL/min



f_{CO_2} 0.25

0.33

0.50



S_{CO_2} 0.060

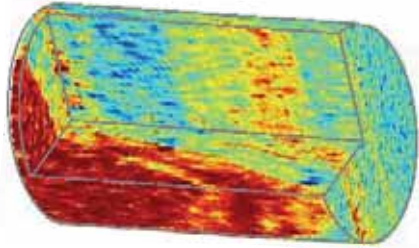
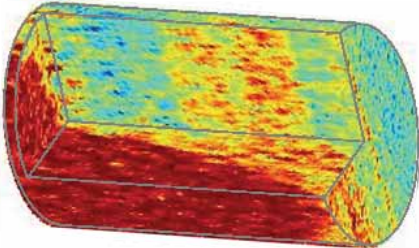
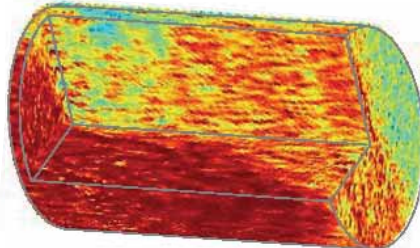
0.152

0.205

f_{CO_2} 0.60

0.72

1



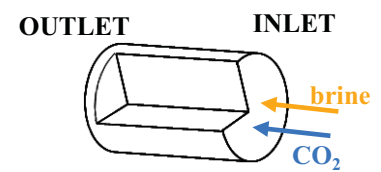
CO₂ saturation

S_{CO_2} 0.273

0.341

0.430

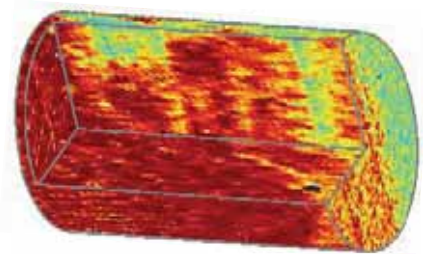
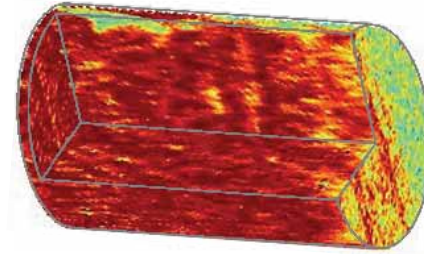
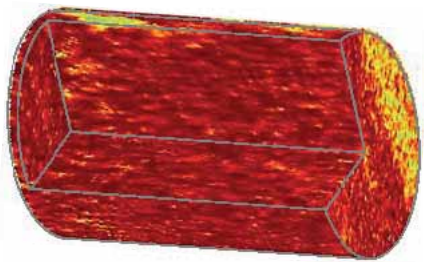
- Results -
 Total flow rate = 1.2 mL/min



f_{CO_2} 0.25

0.33

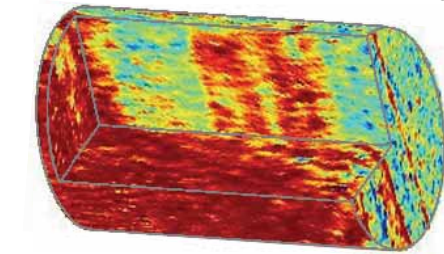
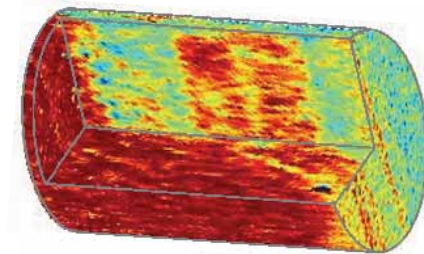
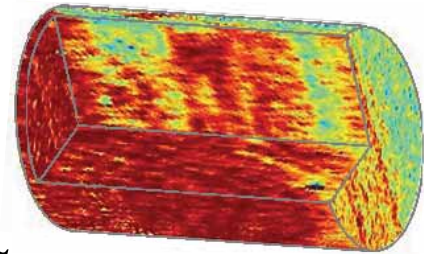
0.50



S_{CO_2} 0.054

0.133

0.209



f_{CO_2} 0.60

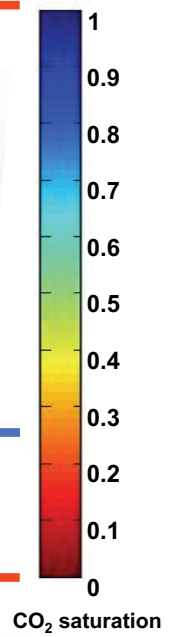
0.79

1

S_{CO_2} 0.227

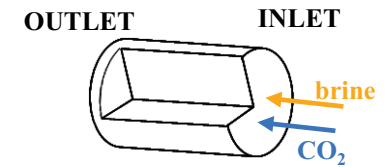
0.269

0.380



- Results -

Total flow rate = 0.5 mL/min

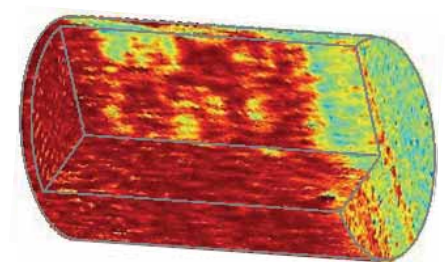
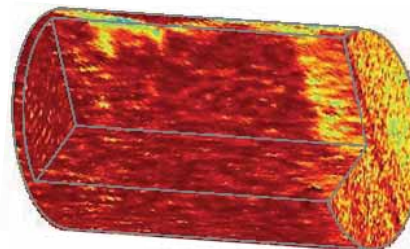
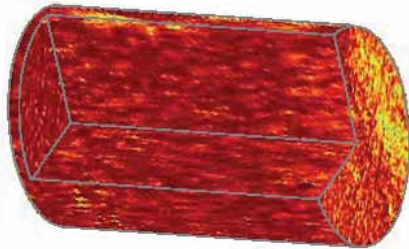
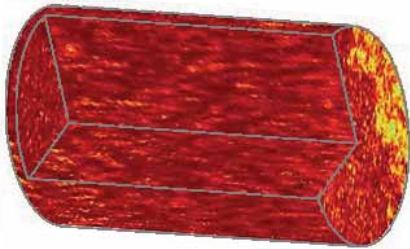


f_{CO_2} 0.16

0.30

0.42

0.60



S_{CO_2} 0.019

0.045

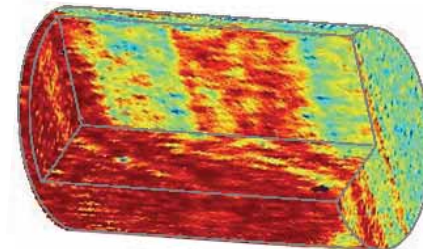
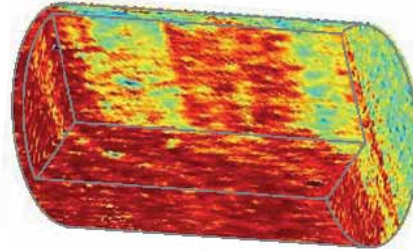
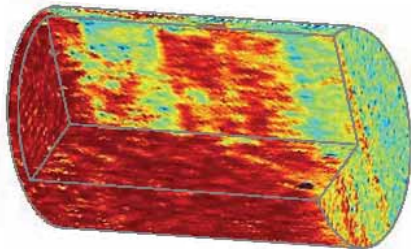
0.105

0.177

f_{CO_2} 0.74

0.84

1



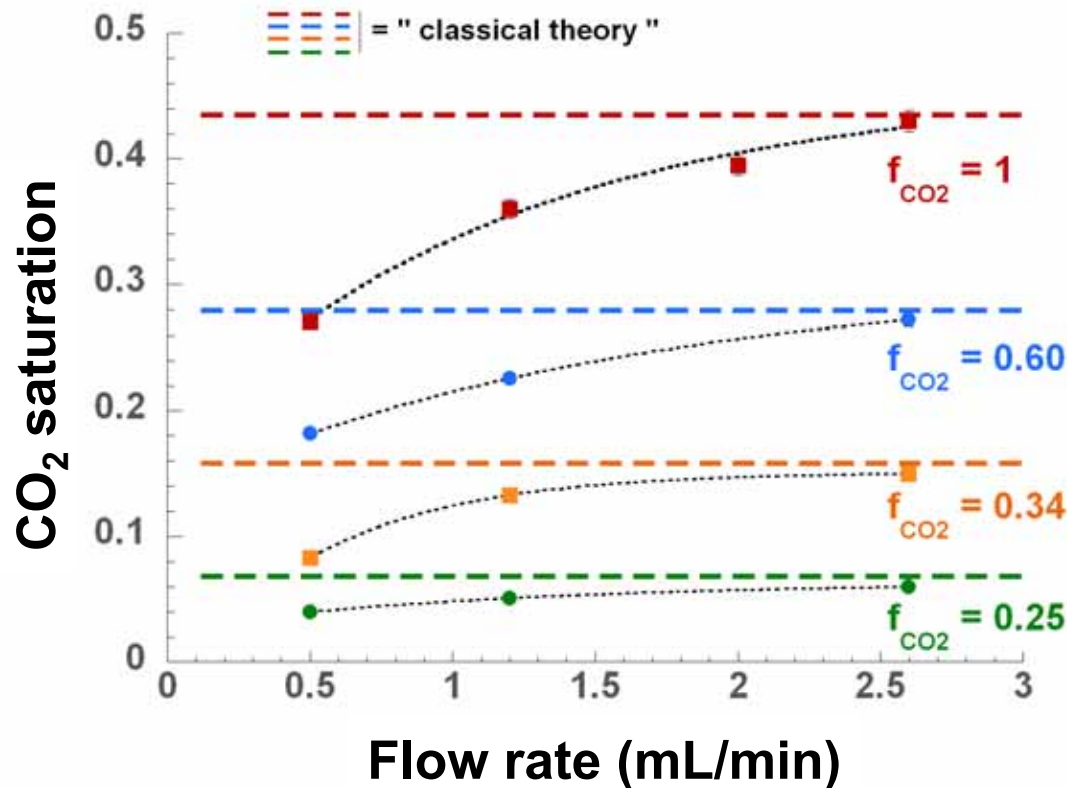
S_{CO_2} 0.233

0.244

0.271

- Results -

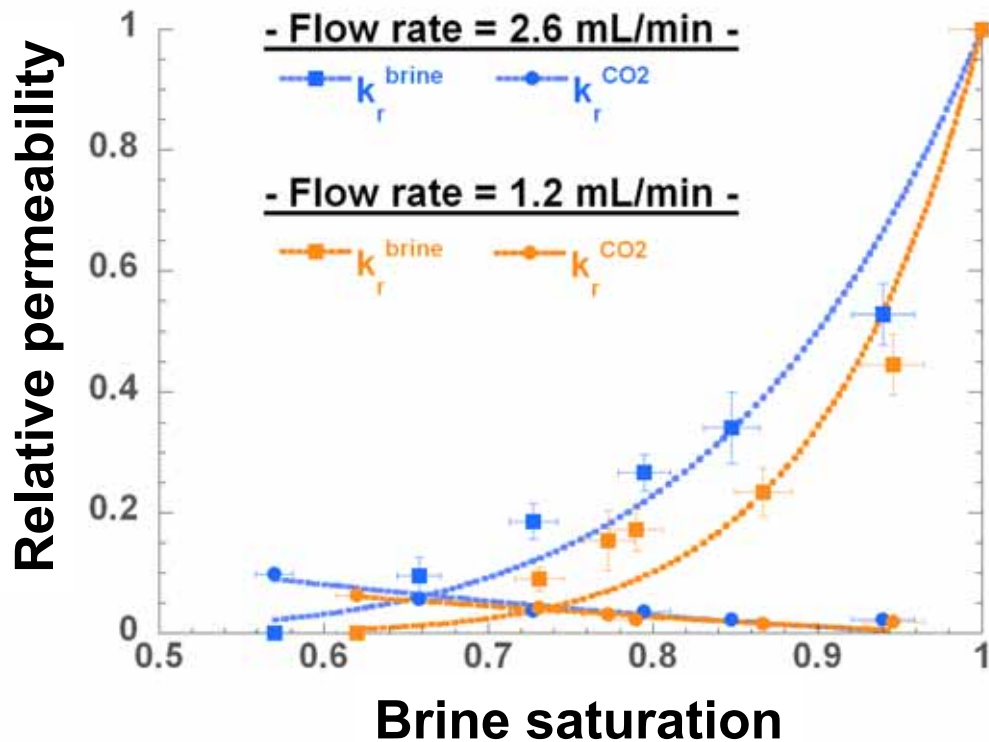
The CO₂ saturation is flow rate dependant



- At any given fractional flow the CO₂ saturation is a function of the flow rate
- The higher the flow rate, the higher the CO₂ saturation
- Results not consistent with classical multi-phase flow theory where saturation – and thus relative permeability – are independent of flow rate

- Results -

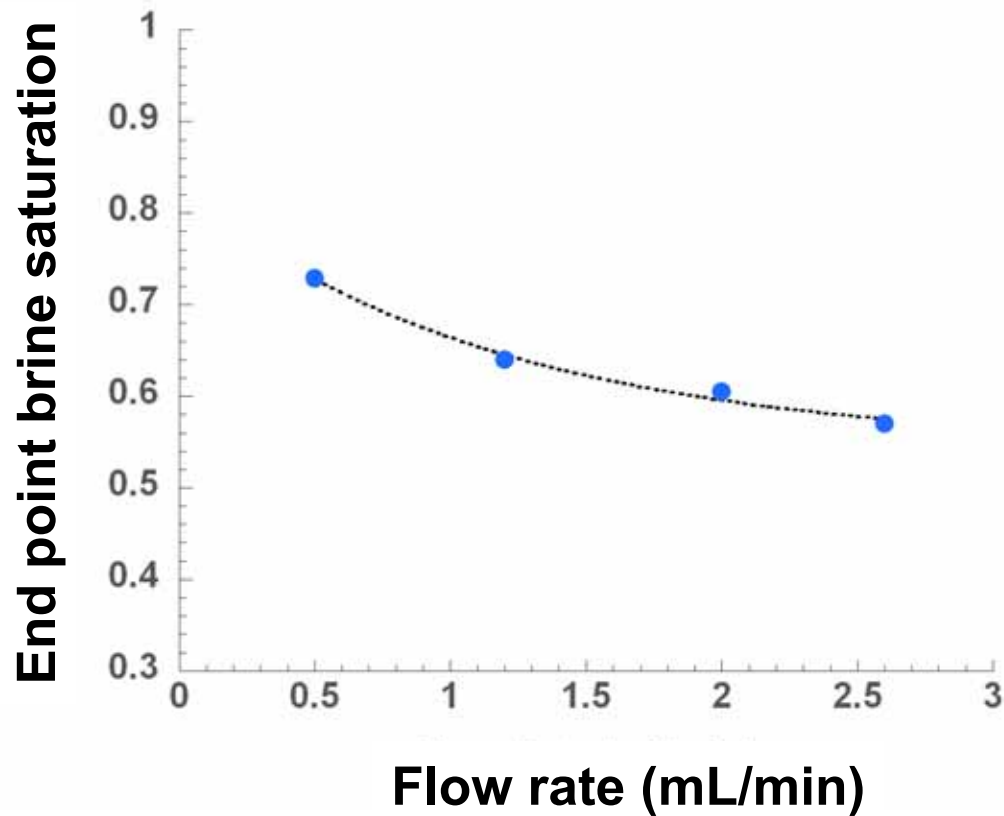
The Relative Permeability curve is flow rate dependant



- Same general trend
- Global shift between the two curves
- The lower the flow rate, the lower the relative permeability

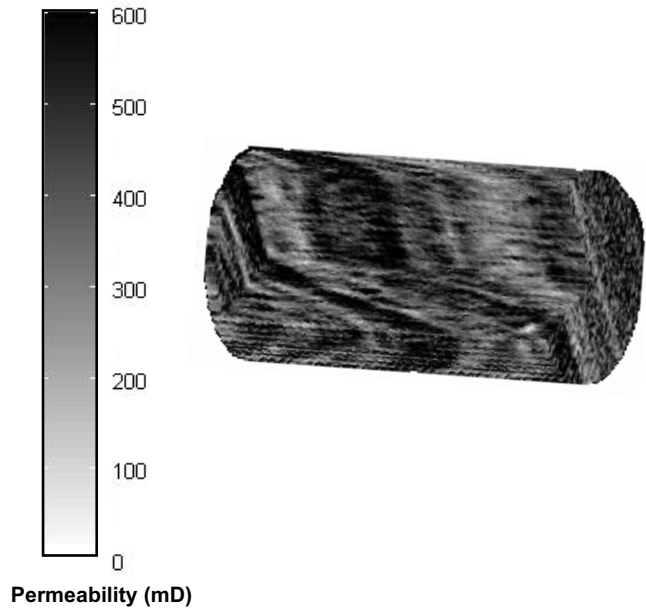
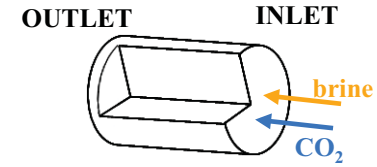
- Results -

The end-point brine saturation is flow rate dependant



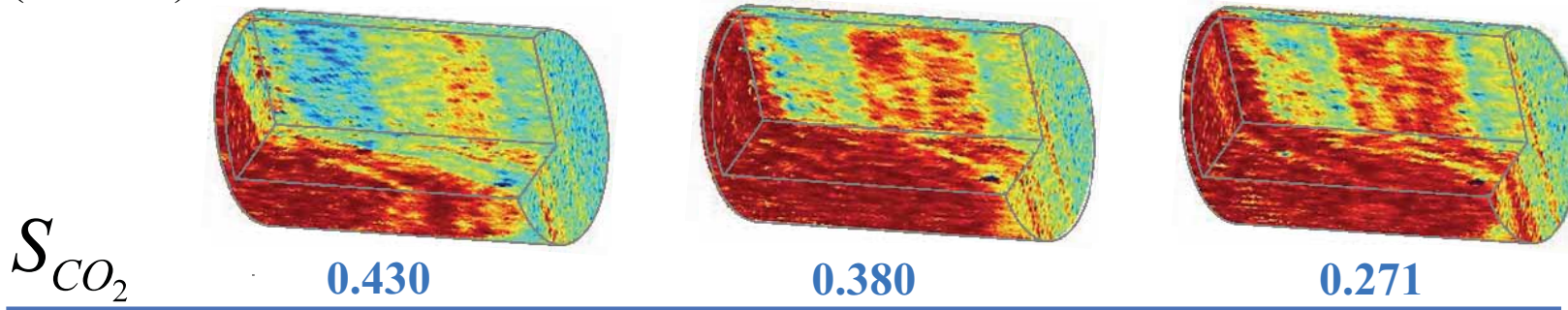
- Strong variations of the end point brine saturation
- Unusually high values
- Asymptotic value for high flow rates

- Results -
Link Permeability - Saturation??



- High permeability paths correspond to high CO₂ saturation close to inlet
- Elsewhere the correlation Permeability – Saturation is poor due to non connected high permeability pathways

Flow rate (mL/min) 2.6 1.2 0.5





- CONCLUSIONS -



- We built a new core flooding experimental setup
- The setup allows us to continuously inject CO₂ and Brine at reservoir conditions



- CONCLUSIONS (2) -



- The first experiments confirm the predicted dependence of CO₂ saturations
- The spatial variations of the permeability (heterogeneities of the pore structure) play a fundamental role in the distribution of CO₂



- CONCLUSIONS (3) -



- Numerical simulations are needed to better understand these observations
- Sub-core scale permeability maps are needed as input in the simulations



- FUTURE WORK -



- More experiments to confirm and more precisely describe the flow rate effect.
- Experimental investigation of imbibitions, relative permeability hysteresis and capillary trapping
- Image the displacement front
- Measure of the relative permeability curve on “real samples” (e.g Otway project, Australia)

- ACKNOWLEDGMENTS -

- Sally Benson
- Global Climate and Energy Project at Stanford
- Organizing committee of the CCS conference